

Lecture 2

Reaction kinetics simulations, sensitivity and uncertainty analyses

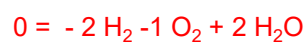
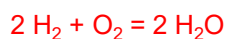
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ELTE Institute of Chemistry



Reaction kinetics basics

**Characterization of chemical changes with
a stoichiometric (overall) equation:**

- properly indicates the ratio of reactants and products
- usually there is no such a real chemical process



$$0 = \sum_j \nu_j A_j$$

$$\nu_1 = -2$$

$$\nu_2 = -1$$

$$\nu_3 = +2$$

$$A_1 = \text{"H}_2\text{"}$$

$$A_2 = \text{"O}_2\text{"}$$

$$A_3 = \text{"H}_2\text{O"}$$

ν_j stoichiometric coefficient
(negative for reactants, positive for products)

Features:

- the order of the species is arbitrary
- the stoichiometric coefficients can be multiplied with the same real number



2

Reaction rate

production rate of a species: $\frac{dY_j}{dt}$

reaction rate: $r = \frac{1}{\nu_j} \frac{dY_j}{dt}$

Y_j is the molar concentration of species A_j e.g. [mole dm⁻³]

in a small domain of concentrations always applicable: $r = k \prod_j Y_j^{\alpha_j}$,

k rate coefficient

α_j reaction order with respect species j

$\alpha = \sum_j \alpha_j$ overall reaction order

3

Complex reaction mechanisms

Almost always there are many simultaneous reaction steps:

$$\sum_j \nu_{ij}^L A_j = \sum_j \nu_{ij}^R A_j$$

A reaction step

can be an elementary reaction (physically occurs this way) or

can be a non-elementary reaction lumped from elementary reactions

ν_{ij}^L matrix of left hand side stoichiometric coefficients
 elementary: sum is not more than 2; zero or positive integer
 non-elementary: zero or positive integer

ν_{ij}^R matrix of right hand side stoichiometric coefficients
 elementary: sum is not more than 2; zero or positive integer
 non-elementary: any real number (can be zero, negative, fraction)

$\Delta \nu_{ij} = \nu_{ij}^R - \nu_{ij}^L$ calculation of the (previous) stoichiometric matrix

4

Kinetic system of differential equations

law of mass action (Guldberg and Waage, 1865):

$$r_i = k_i \prod_j Y_j^{\nu_{ij}^r}$$

k_i rate coefficient of reaction step i

r_i rate of reaction step i

Definition of the kinetic system of differential equations:

$$\frac{dY_j}{dt} = \sum_i \Delta \nu_{ij} r_i; \quad j = 1, 2, \dots, n$$

The kinetic system of differential equations in matrix-vector form:

$$\frac{d\mathbf{Y}}{dt} = \mathbf{v}\mathbf{r}$$

5

Matrices to be mentioned frequently

Initial value problem in reaction kinetics:

$$\frac{d\mathbf{Y}}{dt} = \mathbf{f}(\mathbf{Y}, \mathbf{k}), \quad \mathbf{Y}(t_0) = \mathbf{Y}_0$$

Jacobian: $\mathbf{J} = \left\{ \frac{\partial f_i}{\partial y_j} \right\}$

The Jacobian usually changes with changing concentrations

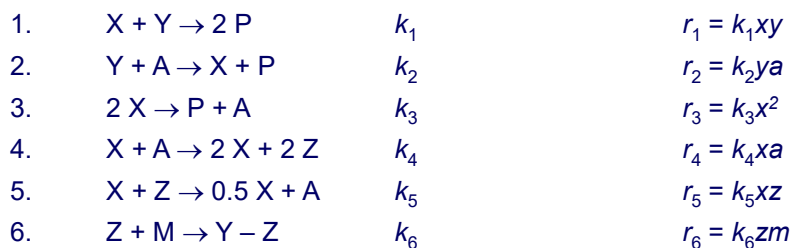
matrix \mathbf{F} : $\mathbf{F} = \left\{ \frac{\partial f_i}{\partial k_j} \right\}$

also depends on the concentrations

6

Kinetic system of differential equations: an example

The Oregonator model of the Belousov-Zhabotinskii oscillating reaction:



$X = \text{HBrO}_2$

$Y = \text{Br}^-$

$Z = \text{Ce}^{4+}$

$A = \text{BrO}_3^-$

$P = \text{HOBr}$

$M = \text{malonic acid}$

The detailed 80-step reaction mechanism could be reduced to this 6 reaction step.

Note, that negative and fractional stoichiometric coefficients are present on the right hand side!

7

Kinetic system of differential equations: an example 2

$X = \text{HBrO}_2$

$Y = \text{Br}^-$

$Z = \text{Ce}^{4+}$

$A = \text{BrO}_3^-$

$P = \text{HOBr}$

$M = \text{malonic acid}$

variable of a diff. equation

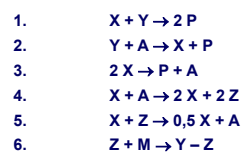
variable of a diff. equation

variable of a diff. equation

constant concentration

product only

constant concentration



$$\frac{dx}{dt} = -1r_1 + 1r_2 - 2r_3 + 1r_4 - 0.5r_5 \quad \Rightarrow \quad \frac{dx}{dt} = -k_1xy + k_2ya - 2k_3x^2 + k_4xa - 0.5k_5xz$$

$$\frac{dy}{dt} = -1r_1 - 1r_2 + 1r_6 \quad \Rightarrow \quad \frac{dy}{dt} = -k_1xy - k_2ya + k_6zm$$

$$\frac{dz}{dt} = +2r_4 - 1r_5 - 2r_6 \quad \Rightarrow \quad \frac{dz}{dt} = 2k_4xa - k_5xz - 2k_6zm$$

8

$\frac{dx}{dt} = -k_1xy + k_2ya - 2k_3x^2 + k_4xa - 0.5k_5xz$ $\frac{dy}{dt} = -k_1xy - k_2ya + k_6zm$ $\frac{dz}{dt} = 2k_4xa - k_5xz - 2k_6zm$			calculation of the Jacobian		
			$\mathbf{J} = \left\{ \frac{\partial f_i}{\partial y_j} \right\}$		
$\frac{\partial \frac{dx}{dt}}{\partial x} = -k_1y - 4k_3x + k_4a - 0.5k_5z$	$\frac{\partial \frac{dx}{dt}}{\partial y} = -k_1x + k_2a$	$\frac{\partial \frac{dx}{dt}}{\partial z} = -0.5k_5x$			
$\frac{\partial \frac{dy}{dt}}{\partial x} = -k_1y$	$\frac{\partial \frac{dy}{dt}}{\partial y} = -k_1x - k_2a$	$\frac{\partial \frac{dy}{dt}}{\partial z} = +k_6m$			
$\frac{\partial \frac{dz}{dt}}{\partial x} = 2k_4a - k_5z$	$\frac{\partial \frac{dz}{dt}}{\partial y} = 0$	$\frac{\partial \frac{dz}{dt}}{\partial z} = -k_5x - 2k_6m$			
			9		

$\frac{dx}{dt} = -k_1xy + k_2ya - 2k_3x^2 + k_4xa - 0.5k_5xz$ $\frac{dy}{dt} = -k_1xy - k_2ya + k_6zm$ $\frac{dz}{dt} = 2k_4xa - k_5xz - 2k_6zm$						calculation of matrix F					
						$\mathbf{F} = \left\{ \frac{\partial f_i}{\partial k_j} \right\}$					
$\frac{\partial \frac{dx}{dt}}{\partial k_1} = -xy$	$\frac{\partial \frac{dx}{dt}}{\partial k_2} = ya$	$\frac{\partial \frac{dx}{dt}}{\partial k_3} = -2x^2$	$\frac{\partial \frac{dx}{dt}}{\partial k_4} = xa$	$\frac{\partial \frac{dx}{dt}}{\partial k_5} = -0.5xz$	$\frac{\partial \frac{dx}{dt}}{\partial k_6} = 0$						
$\frac{\partial \frac{dy}{dt}}{\partial k_1} = -xy$	$\frac{\partial \frac{dy}{dt}}{\partial k_2} = -ya$	$\frac{\partial \frac{dy}{dt}}{\partial k_3} = 0$	$\frac{\partial \frac{dy}{dt}}{\partial k_4} = 0$	$\frac{\partial \frac{dy}{dt}}{\partial k_5} = 0$	$\frac{\partial \frac{dy}{dt}}{\partial k_6} = zm$						
$\frac{\partial \frac{dz}{dt}}{\partial k_1} = 0$	$\frac{\partial \frac{dz}{dt}}{\partial k_2} = 0$	$\frac{\partial \frac{dz}{dt}}{\partial k_3} = 0$	$\frac{\partial \frac{dz}{dt}}{\partial k_4} = 2xa$	$\frac{\partial \frac{dz}{dt}}{\partial k_5} = -xz$	$\frac{\partial \frac{dz}{dt}}{\partial k_6} = -2zm$						
						10					

Properties of kinetic differential equations

- The system of differential equations contains only first order derivatives (dc / dt), which are usually nonlinear functions of the concentrations.
⇒ **first order nonlinear system of differential equations**
- In general, several other concentrations influence the production rate of each species.
⇒ **coupled differential equations**
- The reaction rates differ several orders of magnitude
⇒ **stiff differential equations**
- Simulation results of laboratory experiments do not depend on the wall clock time, **BUT** the results of atmospheric chemical models depend on the actual pressure, temperature and solar radiation ⇒ depend on the physical time.
⇒ **autonomous OR non-autonomous differential equations**
- Some laboratory reactions can be (approximately) spatially homogeneous, but outside the laboratories most chemical reactions are spatially inhomogeneous. In most cases the transport of species and heat have to be taken into account.
⇒ **partial system of differential equations, with chemical source term**

11

Conserved properties

Isolated system:

The total internal energy is constant

Constant volume closed system:

the sum of the concentrations is constant,
if each the change of the number of moles in each reaction step is zero.
e.g. for reaction $\text{H}_2 + \text{Cl}_2 = 2 \text{HCl}$

Closed system, elementary reactions only:

the number of moles of the elements is constant.

The moles of moieties (e.g. benzene ring) can remain constant

Example for conserved properties in a $\text{C}_2\text{H}_4, \text{CH}_4, \text{C}_6\text{H}_6$ mixture:

C-atom $\rightarrow 2 [\text{C}_2\text{H}_4] + 1 [\text{CH}_4] + 6 [\text{C}_6\text{H}_6] = \text{constant}$

H-atom $\rightarrow 4 [\text{C}_2\text{H}_4] + 4 [\text{CH}_4] + 6 [\text{C}_6\text{H}_6] = \text{constant}$

Some linear combinations of the concentrations are constant.

N conserved property:

⇒ the rank of the stoichiometric matrix is lower by N

⇒ the system can be simulated **exactly** with $(n-N)$ variables

12

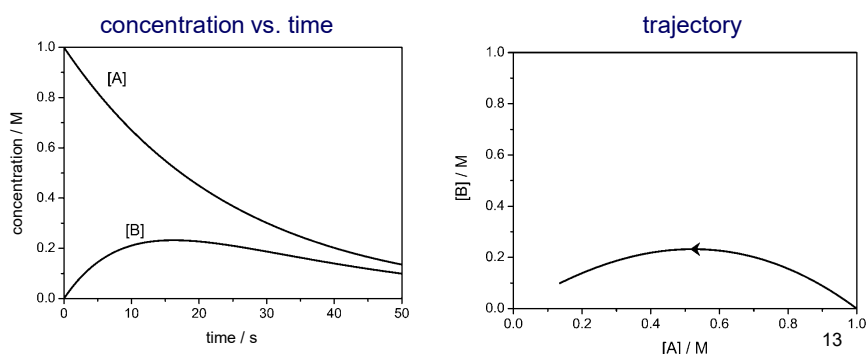
Trajectory

Actual state of the system: a point in the phase space

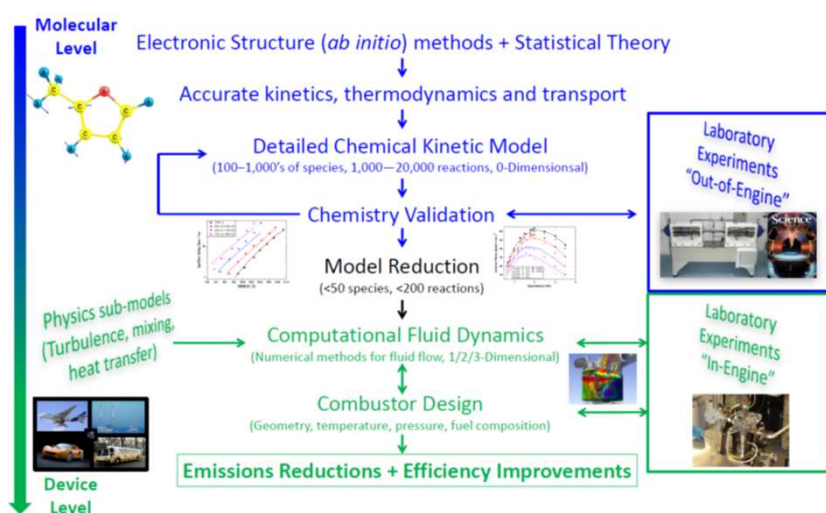
History of events: trace of this point in the phase space (a solid line)

In chemical kinetics this phase space can be the space of concentrations.
This figure does not show time, but can be more interesting than the usual concentration vs. time curves.

Example: reaction $A \rightarrow B \rightarrow$



Hierarchy of combustion models



Henry J. Curran: Developing detailed chemical kinetic mechanisms for fuel combustion
Proc. Combust. Inst., **37**, 57-81 (2019)

14

Source of chemical kinetic data

measured and calculated chemical kinetic data	→	journal publications
data compilation	→	books, data bases. e.g. NIST database www.nist.gov
data evaluation reevaluation and comparison of several articles	→	review articles evaluated/recommended data

15

NIST Chemical Kinetics Database

www.nist.gov

⇒ Databases ⇒ Chemical Kinetics

⇒ NIST Chemical Kinetics Online (<http://kinetics.nist.gov/kinetics/>)

NIST Chemical Kinetics Database

11.700 gas phase reactions

38.000 data entry

12.000 referenced articles

The screenshot displays the NIST Chemical Kinetics Database website. The left sidebar lists various scientific databases under the heading 'NIST Scientific and Technical Databases'. The main content area is titled 'Chemical Kinetics' and provides an overview of the database's scope and history. It mentions that the database is a compilation of kinetic data on gas-phase reactions, version 7.0 (Web Version), release 1.3. A 'Reaction Database Quick Search Form' is visible, allowing users to enter reactant(s) and/or product(s) for a search. The search form includes fields for 'Search', 'Database', and 'Evaluation', along with buttons for 'Submit' and 'Clear'. The page also includes links for 'Home', 'About the database', 'Getting Started', 'Credits and History', and 'Help'.

16

NIST Chemical Kinetics Database 2

Author(s): Gierczak. T.; Talukdar. R.K.; Herndon. S.C.; Vaghjiani. G.L.
 Ravishankara. A.R.
Title: Rate coefficients for the reactions of hydroxyl radicals with methane and deuterated methanes
Journal: J. Phys. Chem. A:
Volume: 101
Page(s): 3125 - 3134
Year: 1997
Reference type: Journal article
Squib: 1997GIE/TAL3125-3134

Reaction: $\text{CH}_4 + \cdot\text{OH} \rightarrow \cdot\text{CH}_3 + \text{H}_2\text{O}$
Reaction order: 2
Temperature: 196 - 420 K
Pressure: 0.13 Bar
Rate expression: $1.76 \times 10^{-13} (\text{cm}^3/\text{molecule s}) (T/298 \text{ K})^{2.82} e^{-1.96 (\pm 0.02 \text{ kcal/mole})/RT}$
Bath gas: He
Data type: Absolute value measured directly
Excitation technique: Flash photolysis (laser or conventional)
Analytical technique: Laser induced fluorescence

17

NIST Chemistry WebBook

Another important Web source:
Webbook (<http://webbook.nist.gov/>)

- thermochemical data for over 7000 compounds
- reaction thermochemistry data for over 8000 reactions.
- IR spectra for over 16.000 compounds.
- mass spectra for over 33.000 compounds.
- UV/Vis spectra for over 1600 compounds.
- gas chromatography data for over 27.000 compounds.
- electronic and vibrational spectra for over 5000 compounds.
- spectroscopic data for over 600 compounds.
- ion energetics data for over 16.000 compounds.
- thermophysical property data for 74 fluids.

18

Traditional way for the development of detailed reaction mechanisms

1. List of elementary reactions is generated
2. Determination of the rate parameters one-by-one:
 - Based on direct measurements
 - Using chemical kinetic databases
 - Calculation/estimation of rate parameters
3. Comparison of the simulation results with the results of indirect measurements.
 - Indirect measurements: time-to-ignition, flame velocity, concentration–time or concentration–distance profiles.
4. Identification of the most important reactions by sensitivity analysis at the experimental conditions.
5. Tuning the rate parameters of the most important reactions, till the model reproduces the experimental data.

No good agreement in most cases

**Different authors tune different parameters
⇒ different mechanisms**

19

Local sensitivity analysis

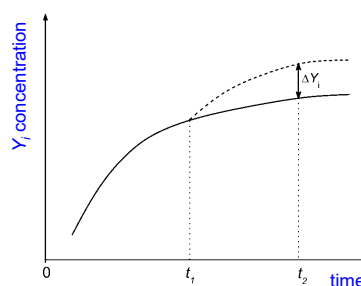
Sensitivity analysis is a family of mathematical methods. It investigates the dependence of the model results on the values of the parameters

Local sensitivity analysis: investigates the effect of the small change of parameters

Local sensitivity coefficients can be investigated by a finite difference approximation:

$$\frac{\partial Y_i}{\partial p_j}(t_1, t_2) \approx \frac{\Delta Y_i(t_2)}{\Delta p_j} = \frac{Y_i(t_2) - Y_i(t_2)}{\Delta p_j}$$

parameter is changed at time t_1
the result is observed at time t_2



T. Turányi: Sensitivity analysis of complex kinetic systems: Tools and applications, *J. Math. Chem.*, **5**, 203-248(1990)

20

Local sensitivity analysis 2

Another approach: Taylor series expansion

$$Y_i(t, \mathbf{p} + \Delta \mathbf{p}) = Y_i(t, \mathbf{p}) + \sum_{j=1}^m \frac{\partial Y_i}{\partial p_j} \Delta p_j + \frac{1}{2} \sum_{k=1}^m \sum_{j=1}^m \frac{\partial^2 Y_i}{\partial p_k \partial p_j} \Delta p_k \Delta p_j + \dots$$

Local sensitivity coefficient: $s_{ik} = \frac{\partial Y_i}{\partial p_k}$

Local sensitivity matrix: $\mathbf{S} = \left\{ \frac{\partial Y_i}{\partial p_k} \right\}$

The effect of parameter changes can be estimated using local sensitivities:

Changing a single parameter: $Y_i(t_2) = Y_i(t_1) + \frac{\partial Y_i}{\partial p_j} \Delta p_j$

Changing several parameters: $\mathbf{Y}'(t_2) = \mathbf{Y}(t_1) + \mathbf{S}(t_1, t_2) \Delta \mathbf{p}(t_1)$

21

Local sensitivity analysis 3

$$\frac{d\mathbf{Y}}{dt} = \mathbf{f}(\mathbf{Y}, \mathbf{p})$$

$$\mathbf{Y}(t_0) = \mathbf{Y}_0$$

Differentiation with respect p_j

$$\frac{d}{dt} \frac{\partial \mathbf{Y}}{\partial p_j} = \mathbf{J} \frac{\partial \mathbf{Y}}{\partial p_j} + \frac{\partial \mathbf{f}}{\partial p_j} \quad \frac{\partial \mathbf{Y}}{\partial p_j}(t_0) = 0 \quad j = 1, 2, \dots, m$$

The same equation with matrix-vector notation:

$$\dot{\mathbf{S}} = \mathbf{J} \mathbf{S} + \mathbf{F}, \quad \mathbf{S}(0) = \mathbf{0}$$

where $\mathbf{J} = \left\{ \frac{\partial f_i}{\partial Y_j} \right\} \quad \mathbf{F} = \left\{ \frac{\partial f_i}{\partial p_k} \right\}$

indirect effect

direct effect

22

Calculation of local sensitivity coefficients

1 Brute force method (finite difference approximation)

$$\frac{\partial Y_i}{\partial p_j}(t_1) \approx \frac{\Delta Y_i(t_2)}{\Delta p_j(t_1)} = \frac{Y_i(t_2) - Y_i(t_1)}{\Delta p_j(t_1)}$$

Δp_j small: large error due to the representation of numbers
 Δp_j large: large error due to nonlinearity

2 Direct method

coupled solution of the kinetic and sensitivity differential equations:

$$\begin{aligned} \frac{d\mathbf{Y}}{dt} &= \mathbf{f}(\mathbf{Y}, \mathbf{p}) & \mathbf{Y}(t_0) &= \mathbf{Y}_0 \\ \frac{d}{dt} \frac{\partial \mathbf{Y}}{\partial p_j} &= \mathbf{J} \frac{\partial \mathbf{Y}}{\partial p_j} + \frac{\partial \mathbf{f}}{\partial p_j} & \frac{\partial \mathbf{Y}}{\partial p_j}(t_0) &= 0 \end{aligned}$$

23

Interpretation of local sensitivity coefficients

$$s_{ik} = \frac{\partial Y_i}{\partial p_k}$$

(Original) local sensitivity coefficients:
 the parameter is changed by one unit
 inspected: the result is changed by how many units
 [unit of result / unit of parameter]

Normalized local sensitivity coefficients:

$$\tilde{s}_{ik} = \frac{p_k}{Y_i} \frac{\partial Y_i}{\partial p_k} = \frac{\partial \ln Y_i}{\partial \ln p_k}$$

investigates relative changes
 How much % change of the result
 due to 1 % change of the parameter?
 dimension free

So far: single parameter is changed
 effect on a single model result is investigated

24

Local uncertainty analysis

If the parameters are correlated, then using the rule of spread of errors the uncertainty of model results can be calculated from the correlation matrix of parameters:

$$\Sigma_Y = S^T \Sigma_p S$$

Here Σ_p is the covariance matrix of parameters, S is the sensitivity matrix and Σ_Y is the covariance matrix simulation results.

If the parameters are uncorrelated, then variance $\sigma^2(y)$ of model result y can be calculated from the variance of parameters: $\sigma^2(p_k)$

$\sigma_k^2(y)$ is the contribution of parameter k to the variance of model result y

$$\sigma_k^2(y) = \sigma^2(p_k) \left(\frac{\partial y}{\partial p_k} \right)^2 \quad \sigma^2(y) = \sum_k \sigma_k^2(y)$$

25

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T. Turányi, L. Zalotai, S. Dóbbé, T. Bérces: Effect of the uncertainty of kinetic and thermodynamic data on methane flame simulation results
Phys. Chem. Chem. Phys., **4**, 2568-2578 (2002)

26

Local uncertainty analysis 2

- Linear approximation of the variance of the model result
- Does not take into account the nonlinear effects
- The result belongs to the nominal set of model parameters
- Realistic results, if the model behaves qualitatively similarly in the whole domain of parameters
- Non-realistic results, if the model is qualitatively different in the various parts of the parameter domain
- Provides separately the contribution of parameters
- Can be calculated fast

27

Applications of local sensitivities

1. **Analysis of models**
 - Estimation of the effect of parameter perturbation
 - Identification of cooperating parameters
2. **Reduction of models**
 - Identification of ineffective parameters; production of a simpler model with less parameters, but almost identical results
3. **Local uncertainty analysis**
 - May replace global uncertainty analysis: less accurate, much faster
4. **Parameter estimation**
 - All gradient methods are based on the (hidden) application of local sensitivity coefficients
 - Identification of effective parameters
 - Experimental design

28

Global uncertainty analysis

Local uncertainty analysis

Provides information at the nominal parameter set

- well applicable, if the model behaves qualitatively similarly in the various regions of parameter space
- exact for linear models

Global uncertainty analysis

the whole physically possible region of parameters is investigated

Global vs. local uncertainty analysis

global methods require much more computer time
acquired information \sim computer time

global uncertainty analysis calculation of the uncertainty of model results from the uncertainty of model parameters

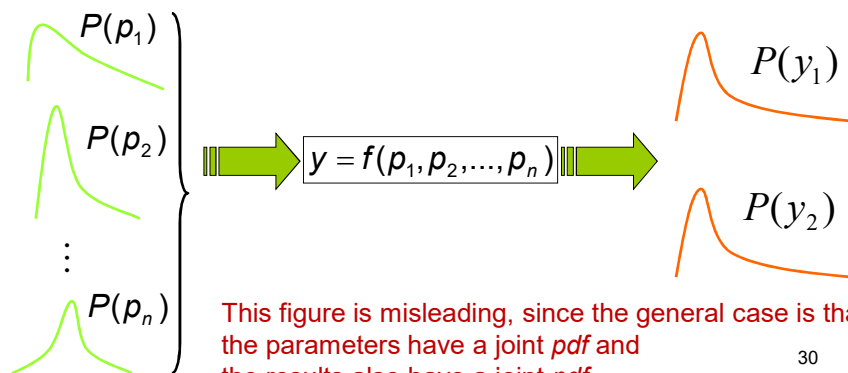
global sensitivity analysis **as above** + identification of the individual contribution of the uncertainty of model parameters ²⁹

Global uncertainty analysis 2

The uncertainty of parameters can be characterized by their probability density function (*pdf*)

The aims of global uncertainty analysis:

1. Calculation of the *pdf* of the results on the basis of the *pdf* of parameters
2. Determination of the contribution of the individual parameters to the standard deviation of model results

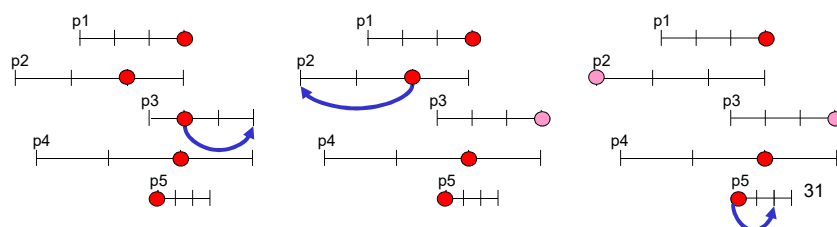


30

Morris method

Screening methods provide approximate information quickly
The Morris method allows the investigation of the effect of large parameter changes

- lower and upper uncertainty limits are assigned to each parameter.
- the uncertainty interval is divided to n parts for each parameter
- random parameter set is selected
- one parameter is changed at each run
- statistical interpretation of the results
- assumes uniform distribution of the parameters
- does not provide the *pdf* of the results
- intermediate computer time

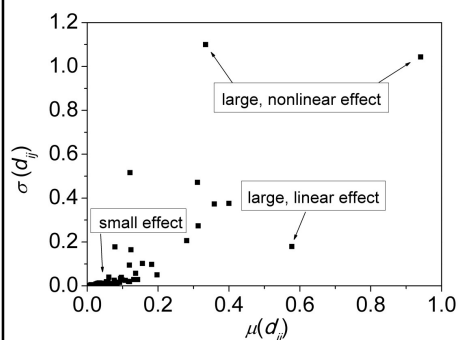


Morris method 2

Value d_{ij} shows the influence of parameter p_j at the random values of all other parameters within their uncertainty interval:

$$d_{ij} = \frac{Y_i(p_1^z, p_2^z, \dots, p_j^z + \Delta, \dots, p_N^z) - Y_i(\mathbf{p}^{z-1})}{|\Delta|}$$

The d_{ij} values are calculated many times in a random calculation and the expected value and standard deviation of d_{ij} is determined.



M. D. Morris:
Factorial sampling plans for preliminary computational experiments.
Technometrics **33**, 161-174 (1991)

F. Campolongo, J. Cariboni, A. Saltelli:
An effective screening design for sensitivity analysis of large models.
Env. Model. Softw. **22**, 1509-1518 (2007)

32

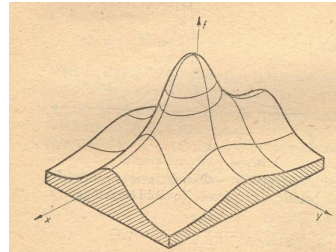
Monte Carlo method

Several thousands of random parameter sets are generated in accordance with the joint *pdf* of the parameters.

The simulations are carried out at these parameter sets.

Statistical analysis of the simulation results:

- determination of the histogram of a result
- calculation of the expected value and standard deviation

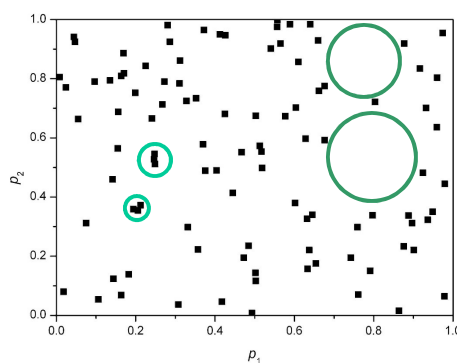


Problems:

- requires much computer time
- it is not easy to trace the effect of individual parameters

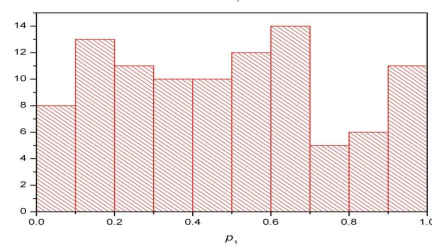
33

Monte Carlo method 2



Generation of 100 (ξ, γ) points
 ξ and γ are random numbers with $[0,1]$ even distribution
 \Rightarrow used for the generation of parameter values p_1 and p_2 , respectively.

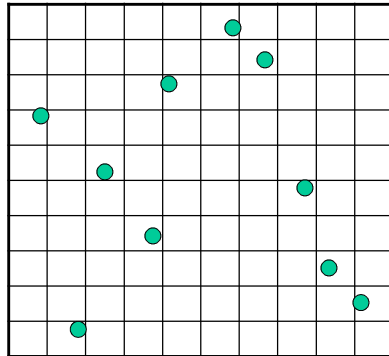
Clogging and empty spots



histogram of p_1

34

Monte Carlo method with Latin hypercube sampling



even distribution

M. D. McKay, R. J. Beckman, W. J. Conover:
A comparison of three methods for selecting
values of input variables in the analysis of
output from a computer code.
Technometrics **42**, 55-61 (2000)

J. C. Helton, F. J. Davis: Latin hypercube
sampling and the propagation of uncertainty
in analyses of complex systems.
Reliab. Engng Syst. Safety **81**, 23-69 (2003)

- stripes („strata”) with equal probability are designated
- within each stripe a point is placed randomly
- if a stripe already contains a point, another point is not placed there ³⁵

Monte Carlo method with Latin hypercube sampling



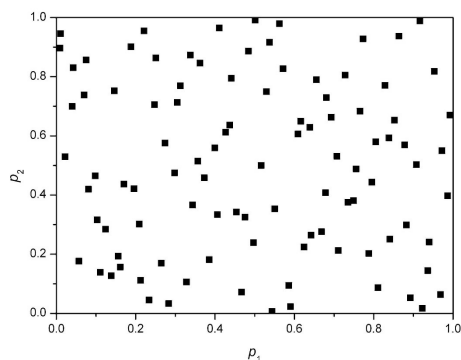
Sir Ronald Aylmer Fisher
(17 February 1890 – 29 July 1962)
British statistician and geneticist.

He has been described as
"a genius who almost single-handedly created the
foundations for modern statistical science,„

His contributions to statistics include the maximum
likelihood, the derivation of various sampling
distributions, founding principles of the design of
experiments, and much more. He developed the
analysis of variance (ANOVA) method.

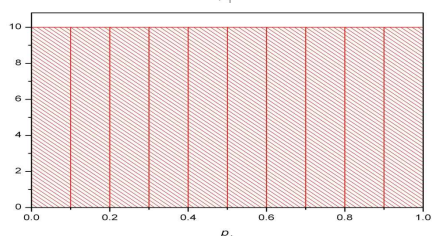
Stained glass window in the dining hall of
Caius College, in Cambridge, commemorating Ronald
Fisher and representing a Latin square,
discussed by him in *The Design of Experiments* ³⁶

Monte Carlo method with Latin hypercube sampling



Generation of 100 (ξ, γ) points
with Latin hypercube sampling

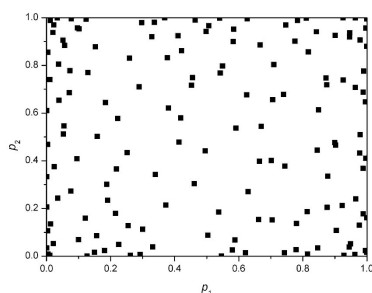
The distribution is
much more even



histogram of p_1

37

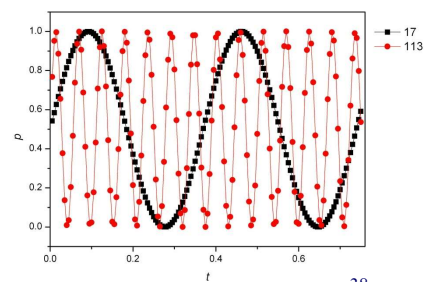
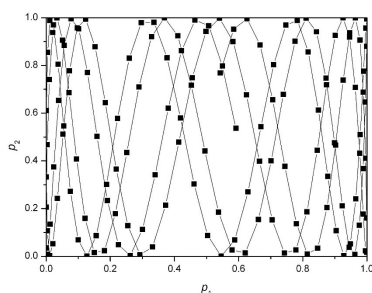
Fourier Amplitude Sensitivity Test (FAST) method



Changing s changing the values of
sin functions having
incommensurable frequency.

The plotted numerical example
shows 150 points and $\Delta s = 0.1$

$x = 0.5 (\sin(17s), \sin(113s)) + 0.5$
 \Rightarrow scaled to a unit square

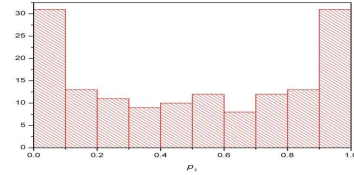
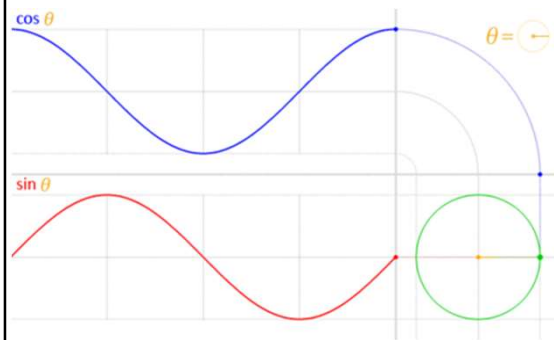
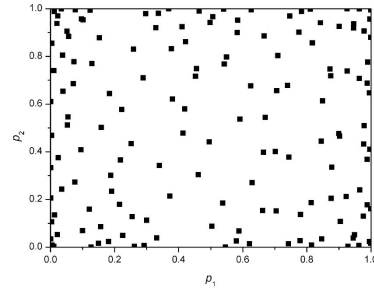


38

Fourier Amplitude Sensitivity Test (FAST) method 2

If the G_j functions are linear, then
(due to the nature of the sine function)
there are more points at the edges

Using appropriate G_j functions,
an *pdf* can be reconstructed
(for independent parameters)



39

Fourier Amplitude Sensitivity Test (FAST) method 4

The simulation results are investigated by Fourier analysis:

$$\sigma^2(Y_i) = 2 \sum_{l=1}^{+\infty} (A_{il}^2 + B_{il}^2)$$

Here $\sigma^2(Y_i)$ is the variance of the result; A_{il} and B_{il} are the Fourier coefficients:

$$A_{il} = \frac{1}{2\pi} \int_{-\pi}^{\pi} Y_i(s) \cos(ls) ds, \quad l = 0, 1, \dots$$

$$B_{il} = \frac{1}{2\pi} \int_{-\pi}^{\pi} Y_i(s) \sin(ls) ds, \quad l = 1, 2, \dots$$

When the Fourier coefficients are calculated at frequency ω_j and its overtones, then the partial variance caused by parameter j is obtained:

$$\sigma_j^2(Y_i) = 2 \sum_{r=1}^{+\infty} (A_{i,r\omega_j}^2 + B_{i,r\omega_j}^2)$$

40

Fourier Amplitude Sensitivity Test (FAST) method 5

partial variance:

$$S_{ij} = \frac{\sigma_j^2(Y_i)}{\sigma^2(Y_i)}$$

This is the fraction of the total variance caused by parameter j

FAST is a slow algorithm; the total number of required simulations:
 $N = 1.2 k^{2.5}$

$N = 21000$ simulations are needed for the investigation of a model having $k = 50$ parameters

The source of extra information for the same amount of computer time:
 Unlike in the MC method, the order of simulations is important;
 patterns are identified in the sequence of simulations

A. Saltelli, R. Bolado: An alternative way to compute Fourier Amplitude Sensitivity Test (FAST)
Comput. Stat. Data Anal. **26**, 445-460 (1998)

41

HDMR method

High Dimensional Model Representation

The simulation results are approximated by a polynomial of the parameters:

$$Y(\mathbf{x}) = Y_0 + \sum_{i=1}^n Y_i(x_i) + \sum_{1 \leq i < j \leq n} Y_{ij}(x_i, x_j) + \dots$$

$Y(x_i)$ the only variable is parameter x_i
 But the function can be even an 8th order polynomial!

$Y(x_i, x_j)$ the variables are parameters x_i and x_j
 Two variables only, but it can also be a high-order polynomial!

T. Ziehn, A. S. Tomlin: GUI-HDMR - A software tool for global sensitivity analysis of complex models.
Environ. Model. Soft. **24**, 775-785 (2009)

GUI-HDMR can be downloaded from website <https://ReSpecTh.hu>

42

HDMR-method 2

random sampling HDMR (RS-HDMR):

Generation of random points in a parameter domain,
fitting polynomials to these points

Approximation with base functions: $Y_i(x_i) = \sum_{r=1}^k \alpha_r^i \varphi_r(x_i)$

Partial variances: $D_i = \sum_{r=1}^{k_i} (\alpha_r^i)^2$

Sensitivity indices: $S_{i_1, \dots, i_s} = \frac{D_{i_1, \dots, i_s}}{D}, \quad 1 \leq i_1 < \dots < i_s \leq m$

43

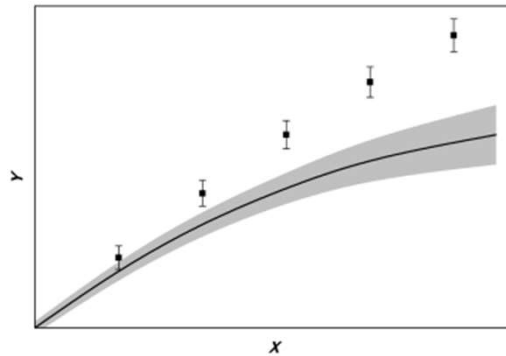
Comparison of the methods

	local	Morris	MC LHS	HDMR
input variance	✓	✓	✓	✓
input <i>pdf</i>	✗	✗	✓	✓
output <i>pdf</i>	✗	✗	⊙	✗
output variance	✓ (linear)	✗	⊙	✓ (biased)
CPU requirement?	⊙ 1	⊙ 2110	3000	16280
Individual contributions	✓ (linear)	✓ (only qualitative)	✗	⊙
global?	✗	⊙ ✓	✓	✓
info about the non-linearities	✗	✓ (only qualitative)	✗	✓

44

Uncertainty analysis: What is it good for?

Is the structure of the model OK?

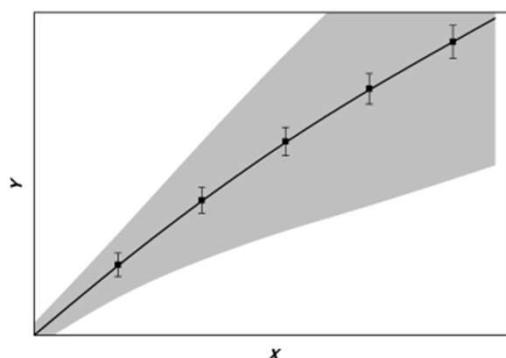


if the experimental data are correct and
if the uncertainty regions of the parameters are well known
BUT the uncertainty regions of measured and simulated results
do not overlap \Rightarrow the structure of the model is bad (wrong equations!)

45

What is it good for? 2

Is the model well established?

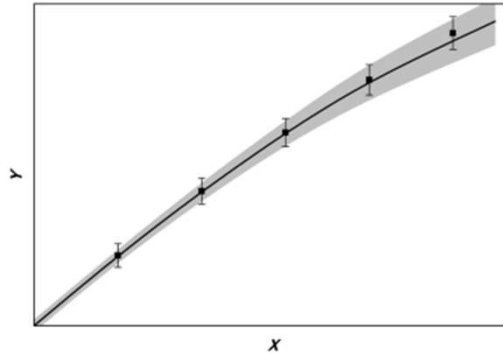


if the uncertainty of the simulated results is much wider than
the uncertainty of the data
 \Rightarrow any simulation result can be obtained with the parameters
 \Rightarrow the model is not useful

46

What is it good for? 3

Are the model parameters well known?



the uncertainty ranges of the data overlap with the uncertainty of the simulation results; the two uncertainty ranges are similar

⇒ the model is OK,

but the uncertainty of the simulation results can be decreased,
if the critical parameters (to be identified by uncertainty analysis)
are determined with smaller uncertainty

47

Summary of uncertainty analysis methods

Local uncertainty analysis

one parameter is changed at a time;
based on partial derivatives
can be calculated quickly

Screening methods

several parameters are changed in wide parameter ranges
intermediate computer time requirement
Morris method

Global uncertainty analysis

all parameters are changed simultaneously
according to their joint *pdf*
requires much computer time
e.g. Monte Carlo method (with Latin hypercube sampling)

48

Example: the uncertainty of methane flame simulation results

The investigated methane flames:

- one dimensional, adiabatic, freely propagating, laminar, premixed stationary flame investigated at equivalence ratios $\varphi = 0.70$ (lean), 1.00 (stoichiometric), and 1.20 (rich)
- cold boundary conditions $p = 1.0$ atm and $T = 298.15$ K

Monitored outputs:

- laminar flame velocity
- maximum temperature
- maximum species concentration of H, O, OH, CH, CH₂

49

Uncertainty analysis of a laminar methane flame

Leeds Methane Oxidation Mechanism:
37 species and 175 reversible reactions
stationary, laminar 1D simulations

37 species: the recommended values of the enthalpies of formation and their variance was calculated from thermodynamic databases

175 reactions: uncertainty parameteres f were collected from Baulch *et al.*

The investigated simulation results:

maximal flame temperature, laminar flame velocity,
maximal concentrations of radicals H, O, OH, CH, CH₂

Uncertainty analysis methods:

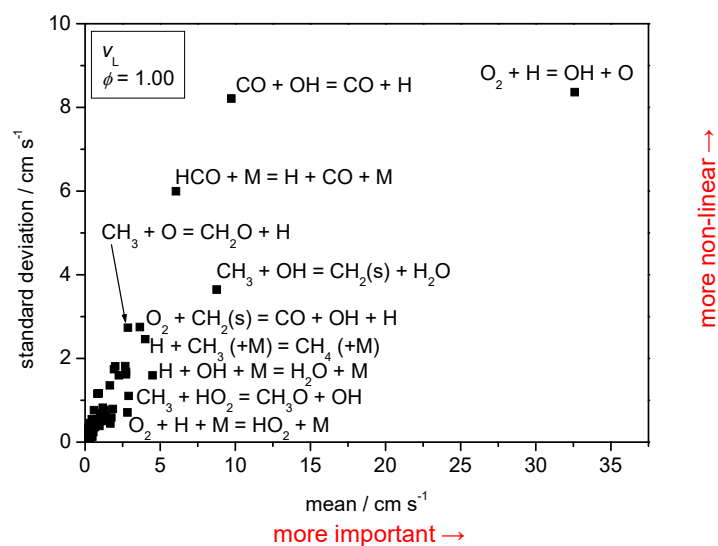
local uncertainty analysis, Morris' method,
Monte Carlo with Latin Hypercube sampling, sensitivity indices

J. Zádor, I. Gy. Zsély, T. Turányi, M. Ratto, S. Tarantola, A. Saltelli: Local and global uncertainty analyses of a methane flame model, *J. Phys. Chem. A*, **109**, 9795-9807 (2005)

50

Morris' method results ($\phi=1$)

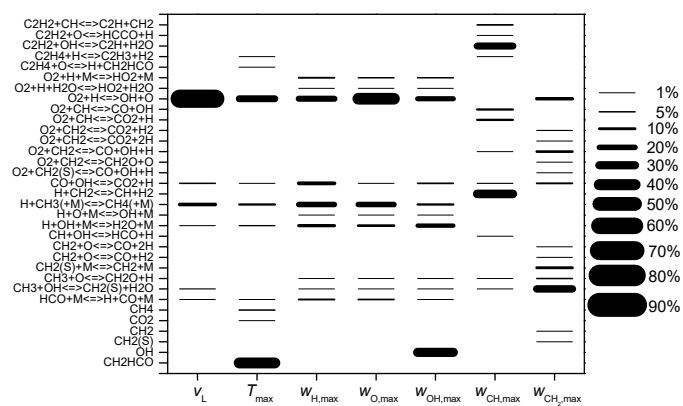
contribution of parameter uncertainties to the uncertainty of the flame velocity



51

Local uncertainty analysis results

% contribution of parameter uncertainties to the uncertainty of the simulated results

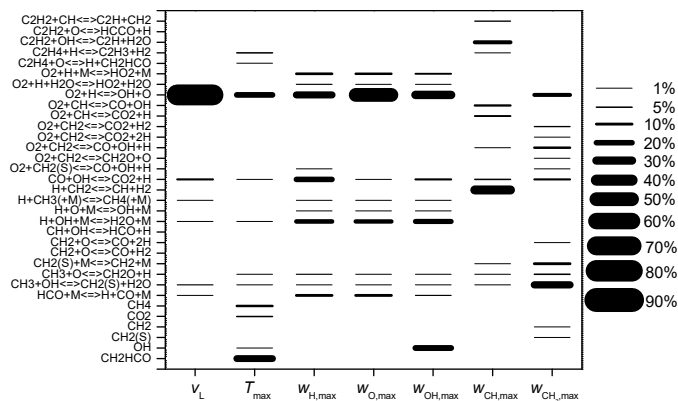


$\phi = 1.0$

52

Uncertainty indices

% contribution of parameter uncertainties to the uncertainty of the simulated results



$$\phi = 1.0$$

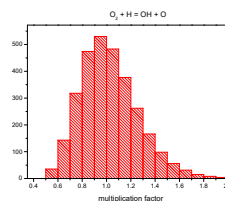
53

Assumed probability density functions of kinetic and thermodynamic parameters

The Monte Carlo and the sensitivity index methods require an assumption on the probability density functions (*pdfs*) of parameters

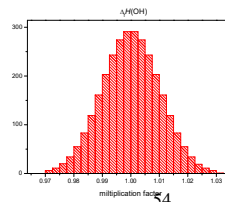
Rate coefficients:

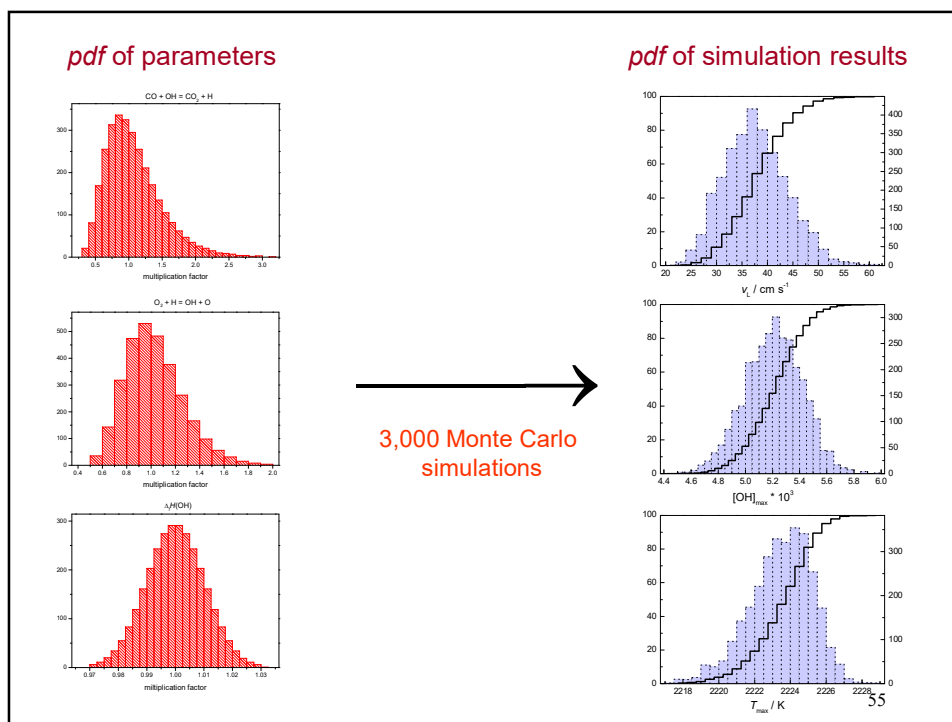
- log-normal distribution
- σ_j was calculated from the f_j uncertainty factor
- the log-normal distribution is clipped at $\pm 3\sigma (\ln k_j)$



Enthalpies of formation:

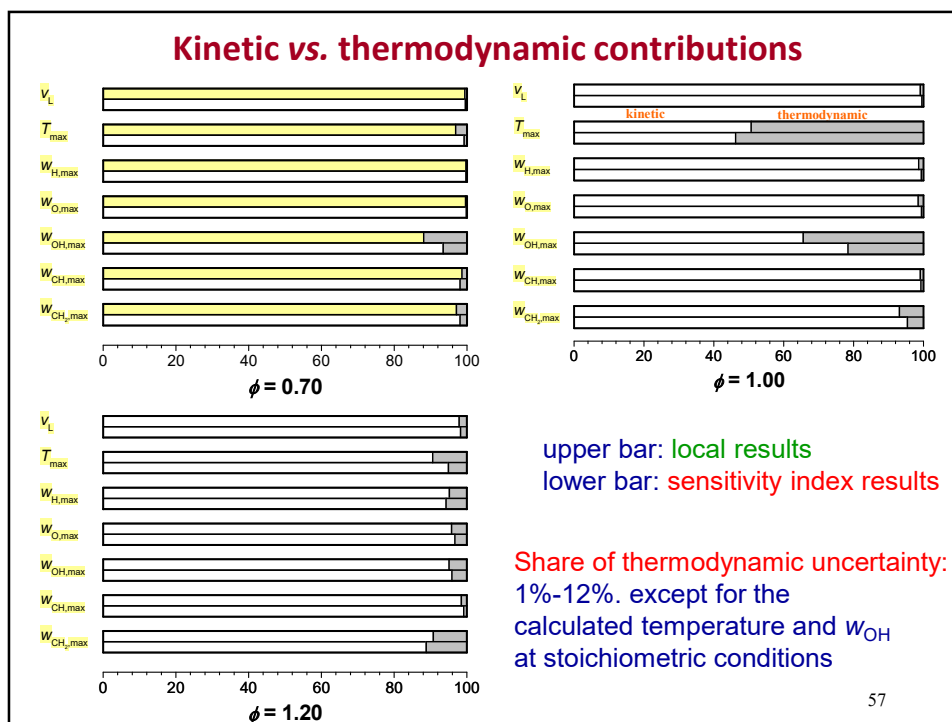
- normal distribution
- σ is assessed on the basis of thermodynamic tables
- the normal distribution is clipped at $\pm 3\sigma$





**Comparison of the results of
local and global (Monte Carlo) uncertainty analyses
for a stoichiometric, stationary, flat methane-air flame**

	result	calculated variances from local Monte Carlo uncertainty analyses	
flame velocity	38.1 cm/s	4.6 cm/s	6.2 cm/s
max. T	2224.2 K	2.8 K	1.7 K
max. w_H	2.14×10^{-4}	14.7%	12.6%
max. w_O	1.74×10^{-3}	13.3%	10.4%
max. w_{OH}	5.27×10^{-3}	3.6%	4.0%
max. w_{CH}	8.07×10^{-7}	46.3%	49.2%
max. w_{CH_2}	2.54×10^{-5}	23.8%	24.0%



Methane flame uncertainty analysis: general conclusions

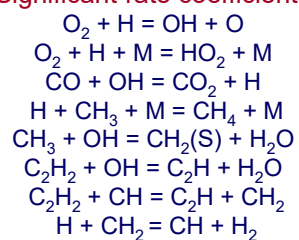
Good agreement between the calculated total variances by the local uncertainty analysis and the Monte Carlo method. (surprise)

Good agreement between the importance of parameters assessed by the local uncertainty analysis and the sensitivity indices. (surprise)

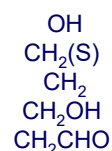
Better simulation results can be achieved, if the rate coefficients of a few reactions and the enthalpies of formation of a few species are known better (= with smaller variance)

These represent a small fraction of the total number of species/reactions.

Significant rate coefficients:



Significant enthalpies of formation:



58

Reaction kinetics branch of the ReSpecTh web site <https://respecth.hu>

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[RKD FILE FORMAT](#)
[COMBUSTION MECHANISMS](#)
[COMPUTER PROGRAMS](#)
[HOW TO?](#)

Reaction kinetics branch of ReSpecTh

Indirect data

The indirect experimental database consists of

- 3239 data files
- 4597 data series
- 151829 datapoints

related to hydrogen, syngas, methanol, ethanol, methane, H₂/O₂/NO_x, ammonia and butanol combustion.

Direct data

The database of direct experimental and theoretical determinations of rate coefficients contains

- 354 data files
- 354 data series
- 6884 datapoints

related to hydrogen, syngas, methanol, ethanol and H₂/O₂/NO_x combustion.

RKD file format

Detailed description of the ReSpecTh Kinetics Data Format.

Computer programs

This section contains the computer programs that were created in or in collaboration with the Chemical Kinetics Laboratory of ELTE.

Combustion mechanisms

This section contains several Chemkin format reaction mechanisms.

How to?

This section provides brief descriptions of the various tasks that can be carried out using the computer programs and experimental data published in this web site.

Experimental and theoretical rate determinations

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Direct experimental and theoretical determinations of rate coefficients

Hydrogen

1749
56
10

Syngas

589
29
5

Methanol

14849
285
18

Ethanol

16808
191
19

H₂/O₂/NO_x

4949
206
21

Legend

Number of datapoints
Number of data series
Number of XML files

Experimental and theoretical rate determinations – Hydrogen

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RE / DIRECT / HYDROGEN

Direct experimental and theoretical determinations of rate coefficients of hydrogen reactions

If you use any of these data files, please cite the appropriate one of the following articles:

Olm, C.; Zsély, I. Gy.; Pálvölgyi, R.; Varga, T.; Nagy, T.; Curran, H. J.; Turányi, T. Comparison of the Performance of Several Recent Hydrogen Combustion Mechanisms. *Combustion and Flame* **2014**, 161 (9), 2219–2234. <https://doi.org/10.1016/j.combustflame.2014.03.006>.

Varga, T.; Nagy, T.; Olm, C.; Zsély, I. Gy.; Pálvölgyi, R.; Valkó, É.; Vincze, G.; Cséhráti, M.; Curran, H. J.; Turányi, T. Optimization of a Hydrogen Combustion Mechanism Using Both Direct and Indirect Measurements. *Proceedings of the Combustion Institute* **2015**, 35 (1), 589–596. <https://doi.org/10.1016/j.proci.2014.06.071>.

Reaction	Number of datapoints	Number of datasets
$\text{H} + \text{O}_2 = \text{O} + \text{OH}$	745	9
$\text{O} + \text{H}_2 = \text{H} + \text{OH}$	338	11
$\text{OH} + \text{H}_2 = \text{H} + \text{H}_2\text{O}$	181	7
$\text{H} + \text{OH} + \text{M} = \text{H}_2\text{O} + \text{M}$	6	3
$\text{H} + \text{O}_2 + \text{M} = \text{HO}_2 + \text{M}$	194	10

Indirect combustion experimental data

RESPECTH HOME INDIRECT DATA DIRECT DATA RKD FILE FORMAT COMBUSTION MECHANISMS COMPUTER PROGRAMS HOW TO?

RE / INDIRECT

Indirect experimental data

Legend

- Number of datapoints
- Number of data series
- Number of XML files

Search	Hydrogen	Syngas
	2430 262 231	4652 423 387
Methanol	Ethanol	Methane
14849 584 287	16808 504 192	11021 1289 1289
H ₂ /O ₂ /NO _x	NH ₃	Methanol/NO _x
4949 332 207	5011 482 306	2574 243 74
	Butanol	
	89347 475 266	

Indirect combustion experimental data Search engine

Search in the indirect experimental database

Initial mixture ☐ Exact match

ⓘ Press enter to insert multiple species, e.g. H2:center>O2:center>

experiment type

temperature or temperature range K pressure or pressure range atm

φ or φ range

Advanced search

Author(s) ☐ Exact match

ⓘ Use family names only. Press enter to insert multiple authors, e.g. Dupuit:center>Lacombe:center>

DOI year or year range

Combustion mechanisms

RESPECTH HOME INDIRECT DATA DIRECT DATA RKD FILE FORMAT COMBUSTION MECHANISMS COMPUTER PROGRAMS HOW TO?

RE / MECHANISMS

Collection of detailed combustion mechanisms

ELTE optimized mechanisms 4 mechanisms 2016-12-05	Hydrogen 20 mechanisms 2013-11-25	Syngas 16 mechanisms 2014-06-24
Methanol 18 mechanisms 2016-12-05	Ethanol 16 mechanisms 2015-10-11	Methane 13 mechanisms 2021-10-29
H₂/O₂/NO_x 18 mechanisms 2019-06-21	NH₃ 40 mechanisms 2023-04-24	Methanol/NO_x 20 mechanisms 2020-08-31
Butanol 24 mechanisms 2021-06-21		

Computer programs

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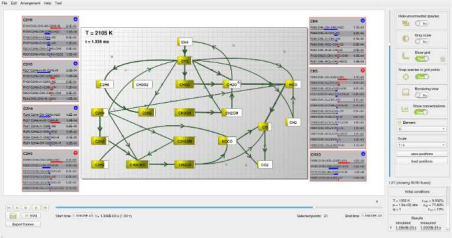
FluxViewer++

Author: Máté Papp

If you use FluxViewer++ please use the following citations:
 Máté Papp, Tamás Turányi: FluxViewer++ (2021), available at <http://respecth.hu/>
 T. Turányi, A. S. Tomlin: Chapter 4 in: *Analysis of kinetic reaction mechanisms*, Springer, 2014

Download

FluxViewer++ is a reaction path visualization tool written in C++ using the Qt graphical interface library. It reads the flux information file generated by Optima++. The program draws the species as boxes and the element fluxes as interconnecting arrows. The boxes and arrows can be moved by the mouse to create a nice arrangement. The arrangement of the boxes and arrows and other visualization settings can be saved into a session file for later reuse. The optimized, nice and chemically meaningful final figure can be saved in the commonly used image formats (PNG, JPEG, BMP) in arbitrary resolution. Development and change of the connections with reaction progress can be inspected as an animation. The frames of the animation can also be saved to create a video or a GIF file.



The screenshot shows the FluxViewer++ application window. It features a central panel displaying a reaction network diagram where species are represented as yellow boxes and fluxes as black arrows. The interface includes a sidebar on the right with a list of programs: FluxViewer++, GUR-HOMR, JPDAP, KINAL, KINALC, MECHMOD, Minimal Spline FR, Optima++, outgen, ReactionKinetics, SAMAP, SEM, UBAC, and uLimits. The main window also has a top menu bar with options like File, Edit, View, and Help.

How to ...

RESPECTH HOME INDIRECT DATA DIRECT DATA RKD FILE FORMAT COMBUSTION MECHANISMS COMPUTER PROGRAMS HOW TO?

How to do useful things?

This section provides brief descriptions of the various tasks that can be carried out using the computer programs and experimental data published in this web site.

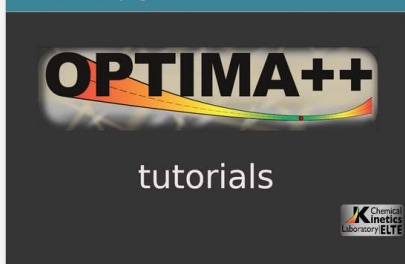
[Tutorial web pages](#) to the applications of the combustion data

[Related tutorial Youtube videos](#)

- Preparation of an RKD xml file
- Solver input files from an RKD file
- Experimental data utilization
- Comparison of the performance of reaction mechanisms
- Optimization of detailed reaction mechanisms

This section provides brief descriptions of the various tasks that can be carried out using the computer programs and experimental data published in this web site.

Tutorial web pages



Related tutorial Youtube videos



Tutorial videos



Software tools developed at the ELTE Chemical Kinetics Laboratory

Tamas Turanyi

4 videos • 292 views • Last updated on Oct 24, 2022



▶ Play all

↺ Shuffle

A series of software tools for the analysis of kinetic reaction mechanisms, collection of large amount of combustion experimental data and other goodies are available at the ReSpecTh web site (www.respecth.hu). These videos demonstrate the possibilities.

Please look at also this web page:



1 Testing a combustion reaction mechanism

Tamas Turanyi • 424 views • 2 years ago



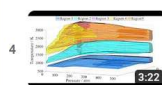
2 Using a computer cluster for testing a combustion reaction mechanism

Tamas Turanyi • 212 views • 2 years ago



3 Encoding combustion experimental data

Tamas Turanyi • 120 views • 2 years ago



4 The chemistry of the ignition of methane - air mixtures

Tamas Turanyi • 194 views • 10 months ago



*Thank you
for your attention!*