

Reaction kinetics modelling

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Please upload the prepared pdf file to the Moodle site of the course!

1. Unzip the rkin_codes.zip package to a folder!

Program 'ckinterp' of the CHEMKIN-II simulation program package creates a binary reaction mechanism file from the CHEMKIN-format text mechanism file. Run ckinterp in a command (cmd) window of a Windows operating system:

```
> ckinterp
```

input:	chem.inp	(text file containing the reaction mechanism)
output 1:	chem.out	(interpreted echo of the input file)
output 2:	chem.bin	(binary file containing the reaction mechanism)

The mechanism provided describes the detonating gas ($\text{H}_2\text{--O}_2$) reaction. The hydrogen combustion mechanism of Varga et al. [T. Varga; T. Nagy; C. Olm; I. G. Zsély; R. Pálvölgyi; É. Valkó; G. Vincze; M. Cserhádi; H. J. Curran; T. Turányi, *Proc. Combust. Inst.* **35** (2015) 589-596] is investigated. For the heterogeneous reactions, the approach of Wang and Law [X. Wang; C. K. Law, *J. Chem. Phys.* **138** (2013) 134305] was adopted, who modelled the wall-loss of species H, O, OH, HO_2 and H_2O_2 as first-order removal reactions. The other species have low sticking coefficients and therefore the corresponding rate coefficients are nearly zero. The wall-loss rate parameters were calculated for a 7.4 cm diameter, spherical quartz reactor using the kinetic theory of gases. The present mechanism has been investigated in the article of Valkó et al. [É. Valkó, T. Varga, A.S. Tomlin, T. Turányi, *Proc. Combust. Inst.* **36**, 681-689 (2017)].

2. Program 'senkin' of the CHEMKIN-II simulation program package carries out spatially homogeneous gas kinetics simulations. Run senkin in a command (cmd) window of a Windows operating system:

```
> senkin <senkin.inp >senkin.out
```

input 1:	chem.bin	(binary file containing the reaction mechanism)
input 2:	senkin.inp	(text file with keywords containing the initial conditions)
output 1:	senkin.out	(echo of input data and the calculated t - T values)
output 2:	tign.out	(text file containing the calculated t, p, T and concentration data; units: s, atm, Kelvin, mole fractions)
output 3:	save.bin	(binary file containing the simulation results)

Files created for making Origin plots; the first line contains the names of the variables:

output 4:	konc_c_molcm3.txt	(t, p, T and concentrations in mol cm^{-3} units)
output 5:	konc_c_x.txt	(t, p, T and concentrations in mole fraction units)
output 6:	konc_c_dbcm3.txt	(t, p, T and concentrations in molecule cm^{-3} units)

Note that “p/Pa” in the output is wrong. It has to be interpreted as “p/atm”.

The meaning of keywords in file „senkin.inp”:

CONV	simulation of a constant volume adiabatic system
TEMP 1250	the initial temperature is 1250 K
PRES 1	the initial pressure is 1 atm
REAC H2 2	ratio of the initial mole fractions of H ₂ , O ₂ and N ₂
REAC O2 1	
REAC N2 3.76	
TIME 1	final time (end of simulation) is 1 second
DELT 1E-9	the initial time step is 10 ⁻⁹ seconds
ATOL 1E-20	absolute tolerance (= largest permitted error) for the calculated mole fractions
ATLS 1E-20	absolute tolerance for the calculated local sensitivity coefficients (not used)
RTOL 1E-09	relative tolerance (= largest relative error in each step) for the mole fractions
RTLS 1E-09	relative tolerance for the calculated local sensitivity coefficients (not used)
END	

Problems to be solved

Name	Neptun code	<i>T</i>	<i>p</i>	<i>φ</i>
Balázs Krisztina	JJS8IN	1000	1	0,65
Burlacu Péter Dániel	UV0XM9	1000	1	0,85
Fábián Lizett	JMHILE	1000	1	1,05
Galanics Kitty Csenge	CE6COC	1000	1	1,25
Gargya Noémi Éva	JJDXN7	1000	1	1,45
Nagy Eszter	RU4P0X	1100	1	0,65
Palik Dezső István	BGG35F	1100	1	0,85
Rácsai Balázs	WM82LC	1100	1	1,05
Radócz Roland	G73MSE	1100	1	1,25
Riznychenko Tetiana	YOJWT5	1100	1	1,45
Sajósi Benedek	PRVEB8	1000	1	0,80
Terbák Enikő Krisztina	D4GW6X	1000	1	1,00
Voigt Inga Maria	IML2PL	1000	1	1,20

1. Carry out simulations using your personal initial conditions above, assuming a constant volume adiabatic system. The initial mixture contains only H₂ and O₂. The final time is 1 second. *φ* is the fuel equivalence ratio, defined as

$$\varphi = (n_{\text{fuel}}/n_{\text{oxidizer}})_{\text{actual}} / (n_{\text{fuel}}/n_{\text{oxidizer}})_{\text{stoichiometric}}$$

Prepare a series of Origin plots that show the 'time vs. temperature' and all 'time vs. species mole fraction' functions. Please select the axes so that all changes are clearly visible. Interpret the shapes of the functions. Some 'time vs. species mole fraction' functions show multiple extrema. What is the chemical explanation of these extrema?

2. Carry out the calculations in such a way that the oxidizer is not pure O₂, but

a) 21% O₂, 79% N₂

b) 21% O₂, 79% Ar

c) 21% O₂, 79% He

d) 21% O₂, 79% H₂O

Use the previous initial temperature T , pressure p and equivalence ratio ϕ .

Interpret the change of ignition delay time and peak temperature, using the following facts:

The constant volume molar heat capacity of the bulk gases (units: J K⁻¹ mol⁻¹)

N₂: 24.37, Ar: 12.48, He: 12.48, H₂O: 32.98

Relative third body efficiency of the bulk gases in reaction step $\text{H} + \text{O}_2 + \text{M} = \text{HO}_2 + \text{M}$

$m(\text{N}_2) = 1$, $m(\text{Ar}) = 0.54$, $m(\text{He}) = 0.65$, $m(\text{H}_2\text{O}) = 12.03$

3. What is the lowest initial temperature where ignition is observed within 1 second using the four mixtures above? Accuracy within 10 K is enough. We consider ignition to occur if the temperature change exceeds 400 K.

4. Using the original H₂/O₂ mixture and initial temperature, calculate the ignition delay time and peak temperature by changing pressure in the interval 10⁻³ atm to 100 atm. Plot the results using at least 15 points, taken equidistantly on a logarithmic pressure scale. Explain the results!

Please upload to the Moodle site a single pdf file that contains all figures, plots and their interpretation.